

APPENDIX

Property Values of Dry air at one atm. pressure

<i>Temperature t °C</i>	<i>Density kg/m³</i>	<i>Coefficient of viscosity μ, kg/ms or Ns/m²</i>	<i>Kinematic Viscosity v, m²/s</i>
- 50	1.584	14.61×10^{-6}	9.23×10^{-6}
- 40	1.515	15.20×10^{-6}	10.04×10^{-6}
- 30	1.453	15.69×10^{-6}	10.80×10^{-6}
- 20	1.395	16.18×10^{-6}	11.61×10^{-6}
- 10	1.342	16.67×10^{-6}	12.43×10^{-6}
0	1.293	17.16×10^{-6}	13.28×10^{-6}
10	1.247	17.65×10^{-6}	14.16×10^{-6}
20	1.205	18.14×10^{-6}	15.06×10^{-6}
30	1.165	18.63×10^{-6}	16.00×10^{-6}
40	1.128	19.12×10^{-6}	16.96×10^{-6}
50	1.093	19.61×10^{-6}	17.95×10^{-6}
60	1.060	20.10×10^{-6}	18.97×10^{-6}
70	1.029	20.59×10^{-6}	20.02×10^{-6}
80	1.000	21.08×10^{-6}	21.09×10^{-6}
90	0.972	21.48×10^{-6}	22.10×10^{-6}
100	0.946	21.87×10^{-6}	23.13×10^{-6}
120	0.898	22.85×10^{-6}	25.45×10^{-6}
140	0.854	23.73×10^{-6}	27.80×10^{-6}
160	0.815	24.52×10^{-6}	30.09×10^{-6}
180	0.779	25.30×10^{-6}	32.49×10^{-6}
200	0.746	25.99×10^{-6}	34.85×10^{-6}
250	0.674	27.36×10^{-6}	40.61×10^{-6}
300	0.615	29.71×10^{-6}	48.20×10^{-6}

1 Ns/m² = 0.102 kgf/m² = 0.1 Poise, $\beta = 1/T$, T in K

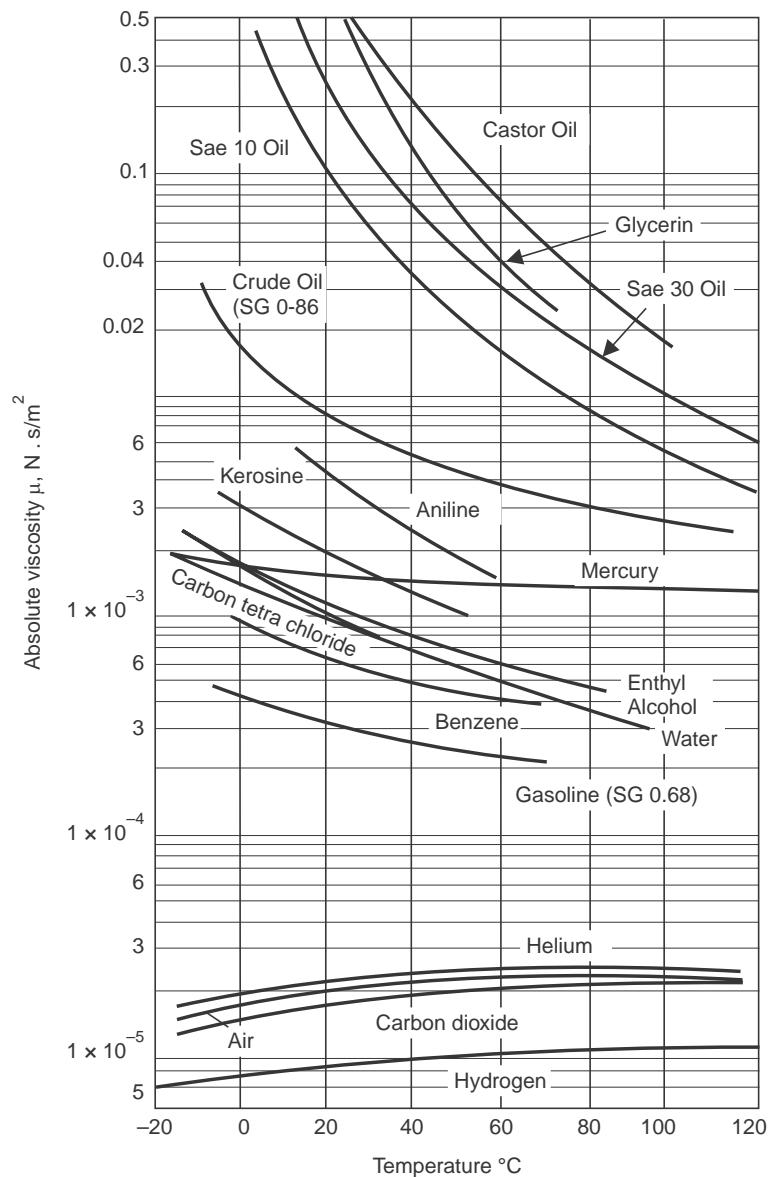
Property Values of Water in Saturated State

<i>Temperature t °C</i>	<i>Density kg/m³</i>	<i>Kinematic Viscosity v, m²/s</i>
0	1002	1.788×10^{-6}
20	1000	1.006×10^{-6}
40	995	0.657×10^{-6}
60	985	0.478×10^{-6}
80	974	0.364×10^{-6}
100	961	0.293×10^{-6}
120	945	0.247×10^{-6}
140	928	0.213×10^{-6}
160	909	0.189×10^{-6}
180	889	0.173×10^{-6}
200	867	0.160×10^{-6}
220	842	0.149×10^{-6}
240	815	0.143×10^{-6}
260	786	0.137×10^{-6}
280	752	0.135×10^{-6}
300	714	0.135×10^{-6}

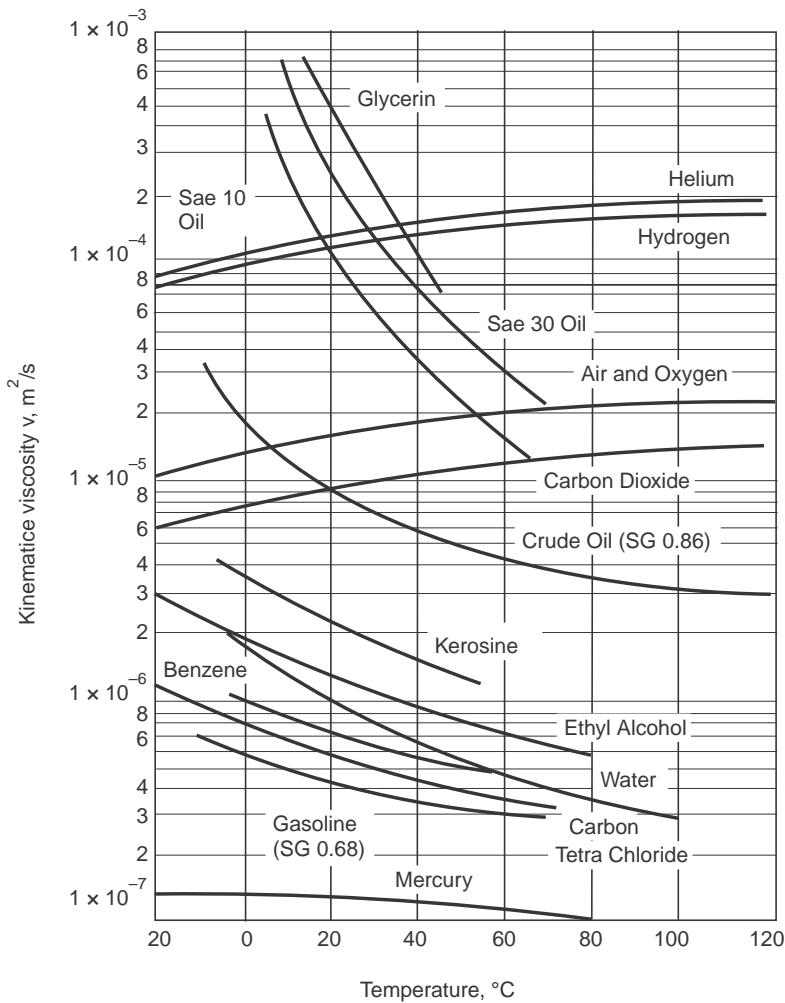
$\beta = (\text{change in density}/\text{change in temp.}) (1/\text{density})$

$\mu = \text{density} \times \text{kinematic viscosity}$, $1 \text{ Ns/m}^2 = 0.102 \text{ kgf/m}^2 = 0.1 \text{ Poise}$

$v = 1 \text{ m}^2/\text{s} = 3600 \text{ m}^2/\text{hr}$



Absolute Viscosity of common fluids at 1 atm.



Kinematic Viscosity of common fluids at 1 atm.

UNIT CONVERSION CONSTANTS

Quantity	SI to Metric	Metric to SI
Force	$1 \text{ N} = 0.1019 \text{ kg}_f$	$1 \text{ kg}_f = 9.81 \text{ N}$
Pressure	$1 \text{ N/m}^2 = 10.19 \times 10^{-6} \text{ kg}_f/\text{cm}^2$ $1 \text{ bar} = 1.0194 \text{ kg}_f/\text{cm}^2$	$1 \text{ kg}_f/\text{cm}^2 = 98135 \text{ N/m}^2, (\text{Pascal})$ $1 \text{ kg}_f/\text{cm}^2 = 0.9814 \text{ bar}$
Energy (heat, work)	$1 \text{ kJ} = 0.2389 \text{ kcal}$ $1 \text{ Nm} (= 1\text{J}) = 0.1019 \text{ kg}_f \text{ m}$ $1 \text{ kW hr} = 1.36 \text{ hp hr}$	$1 \text{ kcal} = 4.186 \text{ kJ}$ $1 \text{ kg}_f \text{ m} = 9.81 \text{ Nm}, (\text{J})$ $1 \text{ hp hr} = 0.736 \text{ kW hr}$
Power (metric)	$1 \text{ W} = 1.36 \times 10^{-3} \text{ hp}$	$1 \text{ hp} = 736 \text{ W}$
Heat flow	$1 \text{ W} = 0.86 \text{ kcal/hr}$	$1 \text{ kcal/hr} = 1.163 \text{ W}$
Specific heat	$1 \text{ kJ/kg K} = 0.2389 \text{ kcal/kg } ^\circ\text{C}$	$1 \text{ kcal/kg } ^\circ\text{C} = 4.186 \text{ kJ/kg K}$
Surface Tension	$1 \text{ N/m} = 0.1019 \text{ kg}_f/\text{m}$	$1 \text{ kg}_f/\text{m} = 9.81 \text{ N/m}$
Thermal Conductivity	$1 \text{ W/m K} = 0.86 \text{ kcal/hr m } ^\circ\text{C}$	$1 \text{ kcal/hr m } ^\circ\text{C} = 1.163 \text{ W/m K}$
Convection Coefficient	$1 \text{ W/m}^2 \text{ K} = 0.86 \text{ kcal/hr m}^2 \text{ }^\circ\text{C}$	$1 \text{ kcal/hr m}^2 \text{ }^\circ\text{C} = 1.163 \text{ W/m}^2 \text{ K}$
Dynamic Viscosity	$1 \text{ kg/ms, (Ns/m}^2\text{)} = 0.1 \text{ Poise}$	$1 \text{ Poise} = 10 \text{ kg/ms, (Ns/m}^2\text{), Pa s}$
Kinematic Viscosity	$1 \text{ m}^2/\text{s} = 3600 \text{ m}^2/\text{hr},$ $1 \text{ Stoke} = 10^{-4} \text{ m}^2/\text{s}$	$1 \text{ m}^2/\text{hr} = 2.778 \times 10^{-4} \text{ m}^2/\text{s}$

Universal gas constant $= 8314.41 \text{ J/kg mol K} = 847.54 \text{ mkg}_f/\text{kg mol K} = 1.986 \text{ kcal/kg mol K}$

Gas Constant for Air $= 287 \text{ J/kg K}, \quad c_p = 1005 \text{ J/kg K} \quad = 0.24 \text{ kcal/kg K}$

Stefan-Boltzmann constant $= 5.67 \times 10^{-8} \text{ W/m}^2\text{K}^4 = 4.876 \times 10^{-8} \text{ kcal/hr m}^2 \text{ K}^4$

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